

more of the sulfur-containing and/or nitrogen-containing organic compounds; and

separating at least a portion of the immiscible peracid-containing phase from the reaction mixture; and

recovering a product comprising a mixture of organic compounds containing less sulfur and/or less nitrogen than the oxidation feedstock from the reaction mixture.

9. The process according to claim 1 wherein the oxidation feedstock consists essentially of material boiling between about 200° C. and about 425° C.

14. The process according to claim 12 wherein the treating of recovered organic phase includes contacting all or at least a portion of the recovered organic phase with at least one solid sorbent comprising alumina.

15. The process according to claim 12 wherein the treating of recovered organic phase includes contacting all or at least a portion of the recovered organic phase with at least one immiscible liquid comprising a solvent having a dielectric constant suitable to selectively extract oxidized sulfur-containing and/or nitrogen-containing organic compounds.

19. The process according to claim 12 wherein the treating of recovered organic phase includes contacting all or at least a portion of the recovered organic phase with at least one immiscible liquid comprising an aqueous solution of a soluble basic chemical compound selected from the group consisting of sodium, potassium, barium, calcium and magnesium in the form of hydroxide, carbonate or bicarbonate.